
VLE from an Equation of State

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FUGACITY IN A MIXTURE BY AN EQUATION OF STATE

$$d\underline{G} = \underline{V}dP - \underline{S}dT + \sum_i \left(\frac{\partial \underline{G}}{\partial n_i} \right)_{T,P,n_{j \neq i}} dn_i$$

and noting,

$$d\underline{A} = -Pd\underline{V} - \underline{S}dT + \sum_i \left(\frac{\partial \underline{A}}{\partial n_i} \right)_{T,\underline{V},n_{j \neq i}} dn_i$$

we may substitute

$$\begin{aligned} d\underline{A} &= d\underline{G} - Pd\underline{V} - \underline{V}dP = \underline{V}dP - \underline{S}dT + \sum_i \left(\frac{\partial \underline{G}}{\partial n_i} \right)_{T,P,n_{j \neq i}} dn_i - Pd\underline{V} - \underline{V}dP \\ \Rightarrow -Pd\underline{V} - \underline{S}dT + \sum_i \left(\frac{\partial \underline{A}}{\partial n_i} \right)_{T,\underline{V},n_{j \neq i}} dn_i &= -Pd\underline{V} - \underline{S}dT + \sum_i \left(\frac{\partial \underline{G}}{\partial n_i} \right)_{T,P,n_{j \neq i}} dn_i \end{aligned}$$

Equating coefficients of dn_i

$$\left(\frac{\partial \underline{A}}{\partial n_i} \right)_{T,\underline{V},n_{j \neq i}} = \left(\frac{\partial \underline{G}}{\partial n_i} \right)_{T,P,n_{j \neq i}} = \mu_i(T,P,\underline{V})$$

Referencing to the ideal gas state:

$$\ln(\hat{f}_i/y_iP) = (\mu_i(T,P) - \mu_i^{ig}(T,P))/RT = \left(\frac{\partial(\underline{A} - \underline{A}^{ig})/RT}{\partial n_i} \right)_{T,\underline{V},n_{j \neq i}} - \ln Z$$

K-Values from an Equation of State

To apply this, consider the PR EOS as an example.

$$\frac{A - A^{ig}}{nRT} = -\ln(1 - B/Z) - \frac{A}{B\sqrt{8}} \ln\left(\frac{Z + (1 + \sqrt{2})B}{Z + (1 - \sqrt{2})B}\right) = -\ln(1 - b\rho) - \frac{a}{bRT\sqrt{8}} \ln\left(\frac{1 + (1 + \sqrt{2})b\rho}{1 + (1 - \sqrt{2})b\rho}\right)$$

For “random mixing”, the probability of any “*i-j* interaction” is the same and goes as the product of the “*i-j* concentrations”. This suggests that we could define $A^v = \Sigma\Sigma y_i y_j A_{ij}$ and $B^v = \Sigma y_i B_i$ letting $A_{ij} = \sqrt{A_{ii} A_{jj}}$ by comparison to the form of the energy equation for mixtures (discussed below). Then differentiation (as detailed below) yields

$$\ln\left(\frac{\hat{f}_i^v}{y_i P}\right) = \frac{B_i^v}{B^v} (Z^v - 1) - \ln(Z^v - B^v) - \frac{A^v}{B^v \sqrt{8}} \ln\left(\frac{Z^v + (1 + \sqrt{2})B^v}{Z^v + (1 - \sqrt{2})B^v}\right) \left(\frac{2\Sigma y_j A_{ij}}{A^v} - \frac{B_i^v}{B^v}\right)$$

Note: $A^L = \Sigma\Sigma x_i x_j A_{ij}$ and $B^L = \Sigma x_i B_i$ but the derivation of the fugacity coefficient would be the same and:

$$\ln\left(\frac{\hat{f}_i^L}{x_i P}\right) = \frac{B_i^L}{B^L} (Z^L - 1) - \ln(Z^L - B^L) - \frac{A^L}{B^L \sqrt{8}} \ln\left(\frac{Z^L + (1 + \sqrt{2})B^L}{Z^L + (1 - \sqrt{2})B^L}\right) \left(\frac{2\Sigma x_j A_{ij}}{A^L} - \frac{B_i^L}{B^L}\right)$$

As we saw in the case of pure fluids, there is no fundamental reason to distinguish between the vapor and liquid phases except by the initial guess for *Z*. The equation of state approach encompasses this lack of distinction in a very direct way. To obtain an expression for K_i , it is convenient to define the fugacity coefficients of a mixture as

$$\frac{\hat{f}_i^v}{y_i P} \equiv \hat{\phi}_i^v \quad \text{and} \quad \frac{\hat{f}_i^L}{x_i P} \equiv \hat{\phi}_i^L \quad \Rightarrow \quad \text{Recalling that } \hat{f}_i^v = \hat{f}_i^L \text{ at equilibrium, we find that } K_i = \frac{\hat{\phi}_i^L}{\hat{\phi}_i^v}$$

UNIT III. FLUID PHASE EQUILIBRIA

FUGACITY IN A MIXTURE BY AN EQUATION OF STATE: Density Dependent Formulas

Example. Fugacity coefficient for the virial equation

For pressures to 10 bars, a common method is to use the virial equation given by:

$Z = 1 + B\rho$; where $B = \sum \sum y_i y_j B_{ij}$ and $B_{ij} = \sqrt{B_{ii} B_{jj}}$. Develop an expression for the fugacity coefficient.

$$\ln(\varphi_k) = \left(\frac{\partial(\underline{A} - \underline{A}^{ig}) / RT}{\partial n_k} \right)_{T, \underline{V}, n_{k \neq i}} - \ln Z; \quad \frac{\underline{A} - \underline{A}^{ig}}{nRT} = \int_0^{B\rho} B\rho \frac{dB\rho}{B\rho} = B\rho \Rightarrow \frac{\underline{A} - \underline{A}^{ig}}{RT} = \frac{Bn^2}{V} = \frac{1}{V} \sum \sum n_i n_j B_{ij}$$

Note: For $B_{ij} = \sqrt{B_{ii} B_{jj}}$, $\sum \sum n_i n_j B_{ij} = \left(\sum n_i \sqrt{B_{ii}} \right) \left(\sum n_j \sqrt{B_{jj}} \right) = \left(\sum n_j \sqrt{B_{jj}} \right)^2$

$$\left(\frac{\partial(\underline{A} - \underline{A}^{ig}) / RT}{\partial n_k} \right)_{T, \underline{V}, n_{k \neq i}} = \frac{1}{V} \frac{\partial \left(\sum n_j \sqrt{B_{jj}} \right)^2}{\partial n_k} = \frac{2 \left(\sum n_j \sqrt{B_{jj}} \right)}{V} \frac{\partial \left(\sum n_j \sqrt{B_{jj}} \right)}{\partial n_k}$$

$$\frac{\partial \left(\sum n_j \sqrt{B_{jj}} \right)}{\partial n_k} = \sqrt{B_{kk}} \Rightarrow \ln(\varphi_k) = \frac{2}{V} \sqrt{B_{kk}} \left(\sum n_j \sqrt{B_{jj}} \right) - \ln Z = 2\rho \left(\sum y_j B_{jk} \right) - \ln Z$$

UNIT III. FLUID PHASE EQUILIBRIA

Example. Fugacity coefficient for the van der Waals EOS

The VdW EOS provides a simple but fairly accurate representation of key EOS concepts for mixtures. The main tricks developed for this EOS are the same for other EOS's but the algebra is a little simpler.

$$Z = \frac{1}{1 - b\rho} - \frac{a\rho}{RT}$$

where $a = \sum \sum y_i y_j a_{ij}$; $a_{ij} = \sqrt{a_{ii} a_{jj}}$
 $b = \sum y_i b_i$

Develop an expression for the fugacity coefficient.

Solution

$$\ln(\phi_k) = \left(\frac{\partial(\underline{A} - \underline{A}^{ig}) / RT}{\partial n_k} \right)_{T, \underline{V}, n_{k \neq i}} - \ln Z$$

$$\frac{\underline{A} - \underline{A}^{ig}}{nRT} = \int_0^{b\rho} (Z - 1) \frac{d(b\rho)}{b\rho} = \int_0^{b\rho} \left(\frac{b\rho}{1 - b\rho} - \frac{a}{bRT} b\rho \right) \frac{d(b\rho)}{b\rho} = -\ln(1 - b\rho) - \frac{a}{bRT} b\rho$$

$$\frac{\underline{A} - \underline{A}^{ig}}{RT} = -n \ln(1 - b\rho) - \frac{an^2}{\underline{V}RT} = -n \ln(1 - b\rho) - \frac{\sum \sum n_i n_j a_{ij}}{\underline{V}RT}$$

$$\left(\frac{\partial(\underline{A} - \underline{A}^{ig}) / RT}{\partial n_k} \right)_{T, \underline{V}, n_{k \neq i}} = -\ln(1 - b\rho) + \frac{n}{1 - b\rho} \left(\frac{\partial b\rho}{\partial n_k} \right) - \frac{1}{\underline{V}RT} \frac{\partial(\sum \sum n_i n_j a_{ij})}{\partial n_k}$$

$$b\rho = \frac{n(\sum y_j \sqrt{b_j})}{\underline{V}} = \frac{(\sum n_j \sqrt{b_j})}{\underline{V}} \Rightarrow \frac{\partial b\rho}{\partial n_k} = \frac{b_k}{\underline{V}}$$

Note: For $a_{ij} = \sqrt{a_{ii} a_{jj}}$, $\sum \sum n_i n_j a_{ij} = (\sum n_i \sqrt{a_{ii}})(\sum n_j \sqrt{a_{jj}}) = (\sum n_j \sqrt{a_{jj}})^2$

$$\frac{\partial(\sum \sum n_i n_j a_{ij})}{\partial n_k} = \frac{\partial(\sum n_j \sqrt{a_{jj}})^2}{\partial n_k} = 2\sqrt{a_{kk}} (\sum n_j \sqrt{a_{jj}})$$

$$\ln(\varphi_k) = -\ln(1 - b\rho) + \frac{n}{1 - b\rho} \left(\frac{b_k}{\underline{V}} \right) - \frac{2\sum n_j a_{kj}}{\underline{V}RT} - \ln Z = -\ln(1 - b\rho) + \frac{b_k \rho}{1 - b\rho} - \frac{2\rho \sum x_j a_{kj}}{RT} - \ln Z$$

$$b\rho \equiv \frac{B}{Z}; \quad \frac{a}{bRT} \equiv \frac{A}{B}; \quad \frac{a_{jk}}{a} \equiv \frac{A_{jk}}{A}; \quad \frac{b_k}{b} \equiv \frac{B_k}{B}$$

$$\ln(\varphi_k) = -\ln(Z - B) + \frac{B_k}{Z - B} - \frac{2\sum x_j A_{kj}}{Z}$$

UNIT III. FLUID PHASE EQUILIBRIA

Example. Fugacity coefficient for the PREOS

$$Z = \frac{1}{1 - b\rho} - \frac{a\rho}{RT(1 + 2b\rho - b^2\rho^2)}$$

where $a = \sum \sum y_i y_j a_{ij}$; $a_{ij} = \sqrt{a_{ii} a_{jj}}$
 $b = \sum y_i b_i$

Develop an expression for the fugacity coefficient.

Solution

$$\ln(\phi_k) = \left(\frac{\partial(\underline{A} - \underline{A}^{ig}) / RT}{\partial n_k} \right)_{T, \underline{V}, n_{k \neq i}} - \ln Z$$

From our integration for the pure fluid,

$$\left(\frac{\underline{A} - \underline{A}^{ig}}{nRT} \right) = -\ln(1 - b\rho) - \frac{a}{bRT\sqrt{8}} \ln \left(\frac{1 + (1 + \sqrt{2})b\rho}{1 + (1 - \sqrt{2})b\rho} \right)$$
$$\left(\frac{\underline{A} - \underline{A}^{ig}}{RT} \right) = -n \ln(1 - b\rho) - \frac{an^2}{nbRT\sqrt{8}} \left\{ \ln[1 + (1 + \sqrt{2})b\rho] - \ln[1 + (1 - \sqrt{2})b\rho] \right\}$$

$$\left(\frac{\partial(\underline{A} - \underline{A}^{ig}) / RT}{\partial n_k} \right)_{T,V,n_k \neq i} = -\ln(1-b\rho) + \frac{n}{1-b\rho} \left(\frac{\partial b\rho}{\partial n_k} \right) - \frac{an^2}{nbRT\sqrt{8}} \left\{ \frac{(1+\sqrt{2}) \left(\frac{\partial b\rho}{\partial n_k} \right)}{1+(1+\sqrt{2})b\rho} - \frac{(1-\sqrt{2}) \left(\frac{\partial b\rho}{\partial n_k} \right)}{1+(1-\sqrt{2})b\rho} \right\}$$

$$- \ln \left[\frac{1+(1+\sqrt{2})b\rho}{1+(1-\sqrt{2})b\rho} \right] \left[\frac{\left(\frac{\partial an^2}{\partial n_k} \right)}{nbRT\sqrt{8}} - \frac{an^2}{RT\sqrt{8}} \frac{\left(\frac{\partial nb}{\partial n_k} \right)}{(nb)^2} \right]$$

$$b\rho = \frac{n(\sum x_j \sqrt{b_j})}{\underline{V}} = \frac{(\sum n_j \sqrt{b_j})}{\underline{V}} \Rightarrow \frac{\partial b\rho}{\partial n_k} = \frac{b_k}{\underline{V}}$$

Note: For $a_{ij} = \sqrt{a_{ii} a_{jj}}$, $\sum \sum n_i n_j a_{ij} = (\sum n_i \sqrt{a_{ii}})(\sum n_j \sqrt{a_{jj}}) = (\sum n_j \sqrt{a_{jj}})^2$

$$\frac{\partial(an^2)}{\partial n_k} = \frac{\partial(\sum \sum n_i n_j a_{ij})}{\partial n_k} = \frac{\partial(\sum n_j \sqrt{a_{jj}})^2}{\partial n_k} = 2\sqrt{a_{kk}} \left(\sum n_j \sqrt{a_{jj}} \right)$$

$$\ln(\varphi_k) = -\ln(1-b\rho) - \ln Z + \frac{b_k \rho}{1-b\rho} - \frac{ab_k \rho}{bRT\sqrt{8}} \left\{ \frac{(1+\sqrt{2})}{1+(1+\sqrt{2})b\rho} - \frac{(1-\sqrt{2})}{1+(1-\sqrt{2})b\rho} \right\} \\ - \frac{a}{bRT\sqrt{8}} \ln \left[\frac{1+(1+\sqrt{2})b\rho}{1+(1-\sqrt{2})b\rho} \right] \left[\frac{2\sum x_j a_{jk}}{a} - \frac{b_k}{b} \right]$$

Note:

$$\frac{b_k \rho}{1-b\rho} - \frac{ab_k \rho}{bRT\sqrt{8}} \left[\frac{(1+\sqrt{2})}{1+(1+\sqrt{2})b\rho} - \frac{(1-\sqrt{2})}{1+(1-\sqrt{2})b\rho} \right] = \frac{b_k}{b} \left\{ \frac{b\rho}{1-b\rho} - \frac{ab\rho}{bRT\sqrt{8}} \left[\frac{1}{1+2b\rho-b^2\rho^2} \right] \right\} = \frac{b_k}{b} \{Z-1\}$$

$$\ln(\varphi_k) = -\ln(1-b\rho) - \ln Z + \frac{b_k}{b} \{Z-1\} - \frac{a}{bRT\sqrt{8}} \ln \left[\frac{1+(1+\sqrt{2})b\rho}{1+(1-\sqrt{2})b\rho} \right] \left[\frac{2\sum x_j a_{jk}}{a} - \frac{b_k}{b} \right]$$

$$b\rho \equiv \frac{B}{Z}; \quad \frac{a}{bRT} \equiv \frac{A}{B}; \quad \frac{a_{jk}}{a} \equiv \frac{A_{jk}}{A}; \quad \frac{b_k}{b} \equiv \frac{B_k}{B}$$

$$\ln(\varphi_k) = -\ln(Z-B) + \frac{B_k}{B} \{Z-1\} - \frac{A}{B\sqrt{8}} \ln \left[\frac{Z+(1+\sqrt{2})B}{Z+(1-\sqrt{2})B} \right] \left[\frac{2\sum x_j A_{jk}}{A} - \frac{B_k}{B} \right]$$

Example 10.6. Bubble point pressure from PR EOS

Use the PREOS($k_{ij} = 0$) to determine the bubble point pressure of equimolar solution of nitrogen+methane at 100K.

Solution:

Initial guess $P \approx \sum x_i P_i^{vap} \approx .5*7.851+.5*.340 = 4.1$ bars; $y_1^{is} = .5*7.851/4.1=.96$

Comp	Tc	Pc	ω	Tb	x	p=4.1,y1=.963		p=4.5,y1=.944		p=4.24,y1=.945	
						K	y	K	y	K	y
N2	126.2	33.94	.040	77	.5	1.95	.970	1.796	.898	1.893	.9467
CH4	190.2	46.00	.011	112	.5	.115	.057	.1046	.052	.1097	.0548
							1.027		0.950		1.0015

Note: y_1 for next guess is computed from estimate of y_1 of current guess. For example, $0.944=0.970/1.027$, and $0.945=0.898/0.950$. Note how quickly the estimate for y_1 converges to the final estimate of 0.945.

Example 10.7. Flash of PREOS solutions

A distillation is to produce overhead products having the following compositions:

	Propane	Isobutane	n-Butane
z_i	0.23	0.67	0.10

Suppose only a partial condensation at 320 K and 8 bars. What fraction of liquid would be condensed according to the PREOS ($k_{ij}=0$)?

Solution: Refer back to the same problem for an ideal solution for guess.

$$L/F = 0.75 \Rightarrow x = \{0.1829, 0.7053, 0.1117\} \text{ and } y = \{0.3713, 0.5624, 0.0648\}$$

						$L/F=$	$L/F=$	$L/F=$		
						0.75	0.90	0.867		
C_o	T_c	P_c	ω	z_i	K_i	D_i	D_i	D_i	x_i	y_i
C3	369.8	42.49	0.152	0.23	1.729	-0.142	-0.1563	-.1528	.2097	.3625
iC4	408.1	36.48	0.177	0.67	0.832	0.118	0.1146	0.1153	.6853	.5700
nC4	425.2	37.97	.193	0.10	0.640	0.040	0.0373	0.0378	.1050	.0673
						0.016	-0.004	0.0002	1.000	.9998

For comparison, $L/F = 0.87$ (PR) vs. 0.75 (IS)

	Propane	Isobutane	n-Butane
K_i (PR)	1.727	0.833	0.641
K_i (IS)	2.03	0.80	0.58

Phase Envelope for PREOS

Use the PREOS($k_{ij}=0$) to determine the phase envelope of nitrogen+methane at 150K. Plot P vs. x_{N_2} , y_{N_2} and compare the results from PREOS to the results from the "short-cut" result.

Solution: use the last guess as the initial guess for the next guess. Above 0.5 mole fraction, increment x_{N_2} by 0.02 each time or you will not converge.

