

ME 812

Conductive Heat Transfer

Wilke Mixture Rule

The Chapman-Enskog model can be used for predicting of thermal conductivity of gas mixtures. Using Wilke's approach we have

$$k_{\text{mix}} = \sum_{i=1}^n \frac{x_i k_i}{\sum_{j=1}^n x_j \Phi_{ij}}$$

where

x_i is the mole fraction of the i th component

$$\Phi_{ij} = \frac{\left[1 + \left(\frac{\mu_i}{\mu_j} \right)^{0.5} \left(\frac{MW_j}{MW_i} \right)^{0.25} \right]^2}{\sqrt{8} [1 + (MW_i/MW_j)]^{0.5}}$$

Note that this equation reduces to

$$\Phi_{ii} = 1$$

The μ in the above equation is the dynamic viscosity for the gas, which can be calculated from the Chapman-Enskog model to be

$$\mu = (2.6709 \times 10^{-6}) \frac{\sqrt{MW \cdot T}}{\sigma^2 \Omega_\mu}$$

where Ω_μ is equal to Ω_k .

Example: Thermal Conductivity of Air as a Gas Mixture

We wish to determine the thermal conductivity of air at 500 K treating it as a gas mixture of N₂ (72%) and O₂ (28%).

Solution:

We will use the Chapman-Enskog model with the Wilke mixture rule. We set up the following table:

Gas	MW	σ	ε/κ	$T\kappa/\varepsilon$	Ω_k	μ	k
N ₂	28.013						
O ₂	31.999						

Going to Table 7.1 to obtain σ and ε/κ .

Gas	MW	σ	ε/κ	$T\kappa/\varepsilon$	Ω_k	μ	k
N ₂	28.013	3.798	71				
O ₂	31.999	3.467	107				

Calculating $T\kappa/\epsilon$ and reading Ω_k from Table 7.2.

Gas	MW	σ	ϵ/κ	$T\kappa/\epsilon$	Ω_k	μ	k
N ₂	28.013	3.798	71	7.042	0.8719		
O ₂	31.999	3.467	107	4.673	0.9393		

For the dynamic viscosity and thermal conductivity we will use

$$\mu = (2.6709 \times 10^{-6}) \frac{\sqrt{MW \cdot T}}{\sigma^2 \Omega_\mu}$$

$$k = k_{\text{monatomic}} + 1.32(c_p - 5/2) \frac{R_u}{MW} (2.6709 \times 10^{-6}) \frac{\sqrt{MW \cdot T}}{\sigma^2 \Omega_k}$$

$$k_{\text{monatomic}} = (8.3127 \times 10^{-2}) \frac{\sqrt{T/MW}}{\sigma^2 \Omega_k}$$

The specific heat, c_p , will be calculated from the equations on Table A.11SI. We then obtain

Gas	MW	σ	ϵ/κ	$T\kappa/\epsilon$	Ω_k	μ	k
N ₂	28.013	3.798	71	7.042	0.8719	2.5133×10^{-5}	0.0383
O ₂	31.999	3.467	107	4.673	0.9393	2.9923×10^{-5}	0.0416

We can now apply our mixture rule,

$$k_{\text{mix}} = \sum_{i=1}^n \frac{x_i k_i}{\sum_{j=1}^n x_j \Phi_{ij}}$$

where

$$\Phi_{ij} = \frac{\left[1 + \left(\frac{\mu_i}{\mu_j} \right)^{0.5} \left(\frac{MW_j}{MW_i} \right)^{0.25} \right]^2}{\sqrt{8} [1 + (MW_i/MW_j)]^{0.5}}$$

Then

$$\Phi_{N_2 N_2} = 1$$

$$\Phi_{N_2 O_2} = 1$$

$$\Phi_{N_2 O_2} = 0.9791$$

$$\Phi_{O_2 N_2} = 1.0205$$

Finally, our mixture thermal conductivity is calculated:

$$k_{\text{mix}} = 0.0392 \text{ W/(m}\cdot\text{K)}$$

From Icropera & DeWitt, we find that at 500 K they give an air thermal conductivity of 0.0407 W/(m·K) or a difference of 3.6%. Hence, this is a pretty good approximation.